

1. Suppose a feedback control system represented by the block diagram in figure



- (a) Determine the equivalent transfer function of the system considering as input to R(s) and output to Y(s).
- (b) Determine the equivalent transfer function of the system considering R(s) as input and E(s) as output.
- 2. Assuming that the reference is a step signal and using analytical and computational tools for the feedback control system from the above problem determine:
  - (a) The value of the controlled variable, y(t)
  - (b) The steady state value of the controlled variable,  $y_{ss} = \lim_{t \to \infty} y(t)$
  - (c) The steady state error,  $e_{ss} = \lim_{t \to \infty} e(t)$
  - (d) The transitory error, e(t) in each case.
  - (e) The maximum overshoot,  $M_p$ .
  - (f) The rise time,  $t_r$ .
  - (g) The settling time,  $t_s$ .

Do the above for each of the following cases:

(a) P control (proportional control) on first-order plant:

$$G(s) = \frac{K}{\tau s + 1}, \ C(s) = K_p.$$

(b) PI control (proportional-integral control) on first order plant:

$$G(s) = \frac{K}{\tau s + 1}, \ C(s) = K_p + \frac{K_i}{s}.$$

(c) P control (proportional control) over a second order plant with a pole at the origin (servo system):

$$G(s) = \frac{K}{s(\tau s+1)}, \ C(s) = K_p.$$

(d) PD control (proportional-derivative control) over a second order plant with a pole at the origin (servo system):

$$G(s) = \frac{K}{s\left(\tau s + 1\right)}, \ C(s) = K_p + K_d s.$$

(e) PI control (proportional-integral control) over a second order plant with a pole at the origin (servo system):

$$G(s) = \frac{K}{s(\tau s + 1)}, \ C(s) = K_p + \frac{K_i}{s}.$$

(f) PID control (proportional-integral-derivative control) over a second order plant with a pole at the origin (servo system):

$$G(s) = \frac{K}{s(\tau s+1)}, \ C(s) = K_p + \frac{K_i}{s} + K_d s.$$

(g) P control (proportional control) over a second order plant:

$$G(s) = \frac{Kw_n^2}{s^2 + 2\zeta w_n s + w_n^2}, \ C(s) = K_p$$

(h) PD control (proportional-derivative control) over a second order plant:

$$G(s) = rac{Kw_n^2}{s^2 + 2\zeta w_n s + w_n^2}, \ C(s) = K_p + K_d s$$

(i) PI control (proportional-integral-derivative control) over a second order plant:

$$G(s) = \frac{Kw_n^2}{s^2 + 2\zeta w_n s + w_n^2}, \ C(s) = K_p + \frac{K_i}{s}.$$

(j) PID control (proportional-integral-derivative control) over a second order plant:

$$G(s) = \frac{Kw_n^2}{s^2 + 2\zeta w_n s + w_n^2}, \ C(s) = K_p + \frac{K_i}{s} + K_d s.$$